# Project: LOW PLATINUM LOADING CATALYSTS

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(This presentation does not contain any proprietary or confidential information.)

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#### **OBJECTIVES**

To assist the DOE in developing of fuel cell technologies by providing low-platinum-loading electrocatalysts.

- To demonstrate the possibility of synthesizing novel electrocatalysts for  $O_2$  reduction with a monolayer level Pt loadings.
- To further characterize of the PtRu<sub>20</sub> electrocatalyst for H<sub>2</sub>/CO oxidation and long term tests.
- To gain understanding of the activity of Pt monolayer and the PtRu<sub>20</sub> electrocatalysts.

#### PROJECT SAFETY

- All the work on this project is performed within the controls identified in the Experimental Safety Review (ESR) Form for this Project.
- Personnel have all the training identified by ESR.
- CO sensor installed at the CO tolerance experiment. Hazard evaluation of this experiment was performed.
- •For the work at synchrotron, the safety procedures and the training requirements of NSLS are followed.

**BUDGET** 

TOTAL FUNDING FOR THE PROJECT (FY 02-04): \$624.000

FUNDING IN FY 04: \$250.000

#### TECHNICAL BARRIERS AND TARGETS

The DOE's Technical Targets for Fuel Cell Stack Systems Operating on Hydrogen (Gasoline Reformate)

	year	2003	2005	2010
precious metal loading	g/kW	<2.0	0.6	0.2
durability	hours	>2000	>2000	>5000
CO tolerance (2% air bleed) ppm		50	500	1000



Development of low-Pt-loading electrocatalysts by placing a submonolayer-to-monolayer of Pt on nanoparticles of suitable metals or alloys to obtain electrocatalysts with the following characteristics:

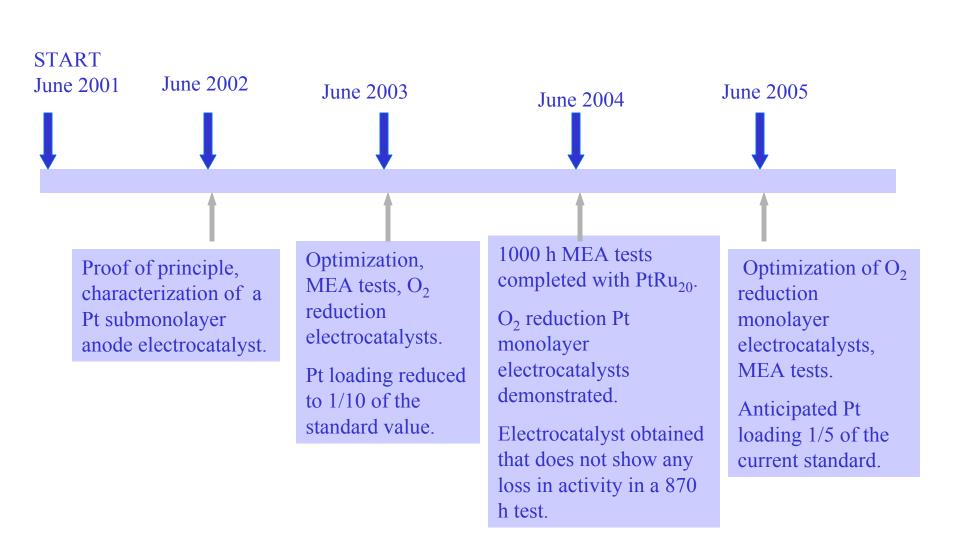
- ultimately reduced Pt loading
- enhanced activity of Pt
- complete utilization of Pt

#### Two methods for Pt monolayer deposition were developed:

- 1. Electroless (spontaneous ) Pt deposition on Ru.
- 2. Pt deposition by replacing a UPD metal adlayer.



#### PROJECT TIMELINE



#### TECHNICAL ACCOMPLISHMENTS



#### **ANODE**

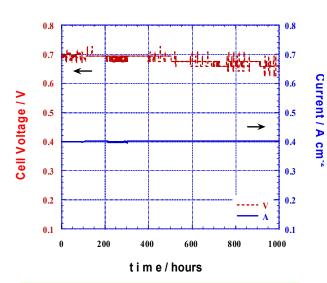
- Stability tests at LANL (F. Uribe) show **no loss of voltage after 870 h** for the PtRu<sub>20</sub> electrocatalyst with 18  $\mu$ g Pt/cm<sup>2</sup> (20% Ru; 2% Pt, 3% air bleed), and small losses after 1000 h with 18  $\mu$ g Pt/cm<sup>2</sup> (10% Ru; 1% Pt, 4% air-bleed) and very small losses in a 600 h test with 19  $\mu$ g Pt/cm<sup>2</sup> (2% air-bleed) of combined CO/H<sub>2</sub> and H<sub>2</sub> operation.
- ➤ The DOE durability target of 2000h for 2005 can be reached with this electrocatalyst.
- ➤ The DOE target for 2005 for noble metals of 0.6 g/kW (0.3 g/kW for anode) is met for Pt: **only 0.063 g Pt/kW is necessary**. If Ru is counted, 0.630 g total metal is needed.

#### **CATHODE**

- $\triangleright$  A Pt monolayer on C-supported metal or metal alloy nanoparticles can be an active catalyst for  $O_2$  reduction.
- ➤ The Pt mass-specific activity of Pt/Pd/C is 5-8 times higher than that of Pt(10%)/C. The (Pt + Pd) mass activity is 2.5 times higher. Fuel cell tests (F. Uribe) are quite promising.
- ➤ A PdCo/C electrocatalyst was synthesized. Its activity is comparable to that of Pt.
- A Pt/AuNi/C electrocatalyst was synthesized whose activity is similar to that of Pt.

#### LONG-TERM FUEL CELL TESTS AT LANL (F. Uribe)



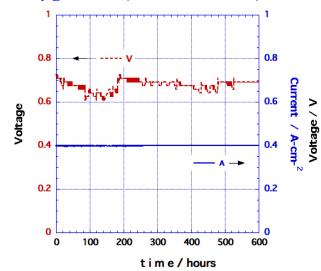


Voltage losses after 1000 hr:

\* with neat H<sub>2</sub>: 40 mV with H<sub>2</sub>+CO+4% air: 60 mV

Cell=50 cm2; T= 80 C; A: 0.19 mg /cm2(10%Ru, 1%Pt) C: 0.23 mg Pt /cm2(20% Pt/C, ETEK) Total run time = 1000 hours at constant current. 710 hours of operation with clean H2 and 290 hours with H2 + 50 ppm CO + 4 % air bleed.

#### 19 μg Pt/cm<sup>2</sup> (10% Ru; 1% Pt)



Voltage losses after 600 hr:

\* with neat H<sub>2</sub>: 20 mV

(0.71-0.69 V)

\* with H<sub>2</sub>+CO+2% air: 20 mV

(0.66-0.64 V)

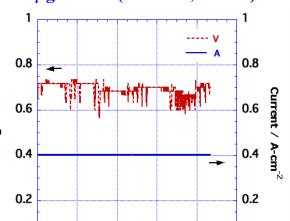
Cell 50 cm<sup>2</sup> cell / T= 80 C

A: 0.19 mg BNL/cm<sup>2</sup> (10% Ru; 1% Pt)

C: 0.22 mg Pt/cm<sup>2</sup> (ETEK)

H<sub>2</sub> 471 hr; H<sub>2</sub> + CO 50 ppm

+2% air bleed, 129 hr



18 μg Pt/cm<sup>2</sup> (20% Ru; 2% Pt)

No voltage losses after 868 hr:

time/hours

600

800

1000

0.701

initial V final V with  $H_2$ : 0.717 0.717

\* with  $H_2$ +CO+3% air:

400

200

0.697

Cell 50 cm<sup>2</sup> cell / T= 80 C

A: 0.20 mg BNL/cm<sup>2</sup> (20% Ru; 2% Pt)

C: 0.24 mg Pt/cm<sup>2</sup> (ETEK)

**Running Mode: 20 A current** 

a) H<sub>2</sub> at @ 1.3 stoich

b) H<sub>2</sub> at @ 1.3 stoich + CO 50 ppm

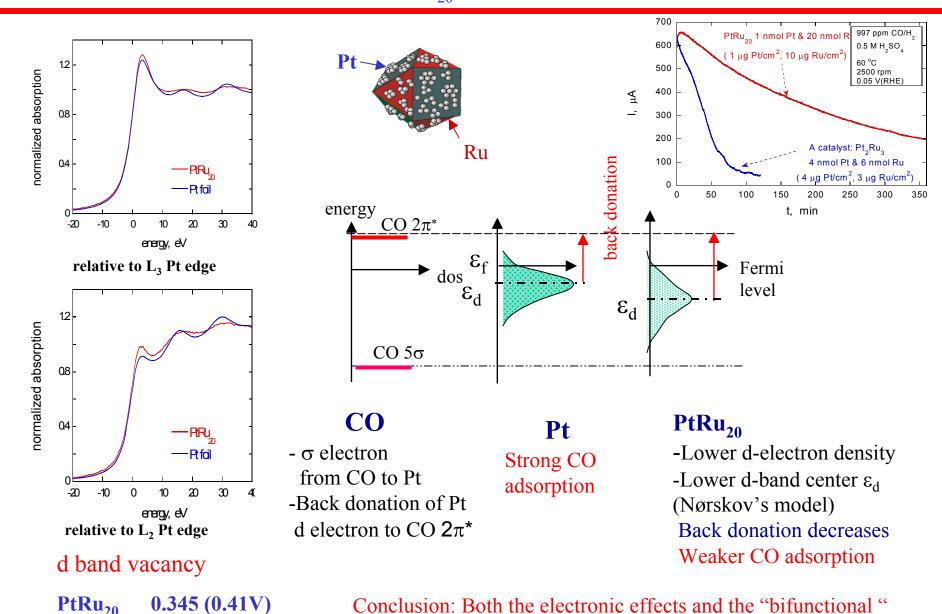
+3% air bleed

Air flow: constant @ 2100 sccm

In addition to CO tolerance, **the very strong surface segregation** of Pt is a key factor in its stability.

#### ELECTRONIC EFFECTS vs. BIFUNCTIONAL MECHANISM IN CO TOLERANCE OF THE PtRu<sub>20</sub> ELECTROCATALYST



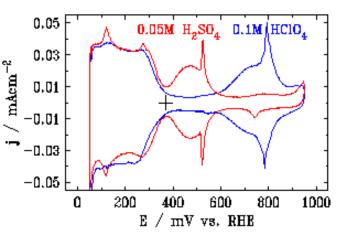


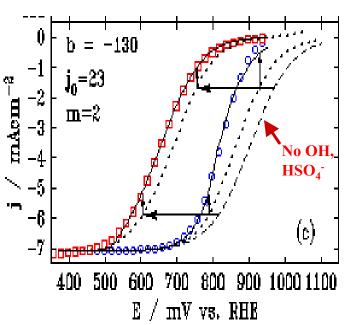
Pt foil

0.30

Conclusion: Both the electronic effects and the "bifunctional" mechanism are operative for this electrocatalyst.







The kinetic currents are calculated as a function of E and the anion adsorption isotherm,  $\theta_A(E)$  using

$$j_k(E) = -j_0 (1 - \gamma_A \theta_A(E))^m$$
  

$$\exp(-2.3(E - E^0 - \varepsilon_A \theta_A(E))/b),$$

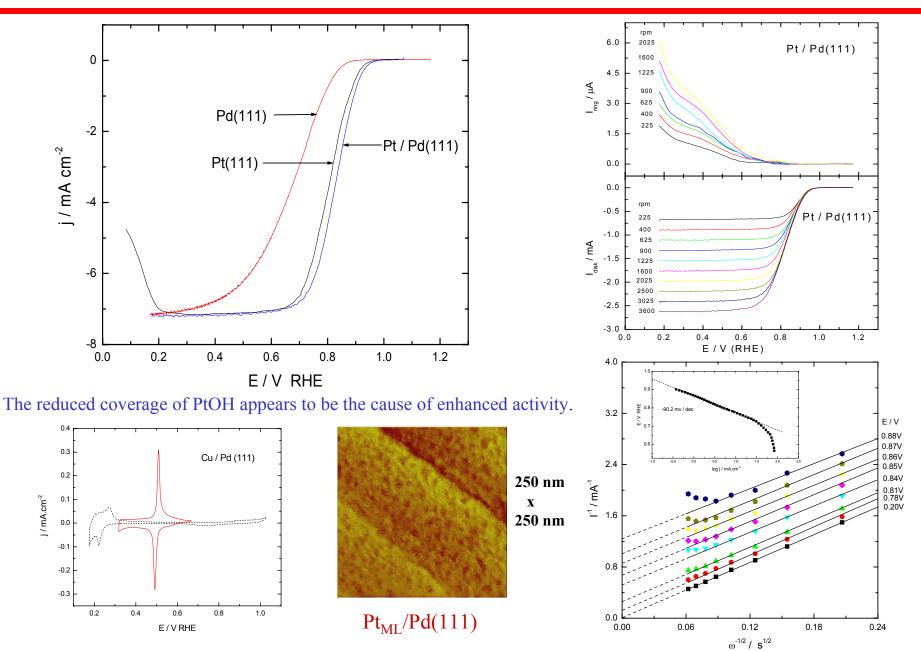
where  $j_0$  and b are the intrinsic kinetic parameters,  $\gamma_A$  is the geometric blocking factor, and  $\varepsilon_A$  is the electronic effect of adsorbed anions

- •The best fits yielded the intrinsic Tafel slope in the range -118 to -130 mV/dec.
- •In addition to site blocking, both OH and bisulfate have a negative electronic effect on ORR kinetics, with the effect of the latter being much stronger.
- The deviation of the apparent Tafel slope in HClO<sub>4</sub> from its intrinsic value can be fully accounted for by the site blocking and electronic effects of adsorbed OH ions, which vary with coverage over the mixed kinetic-diffusion controlled region.

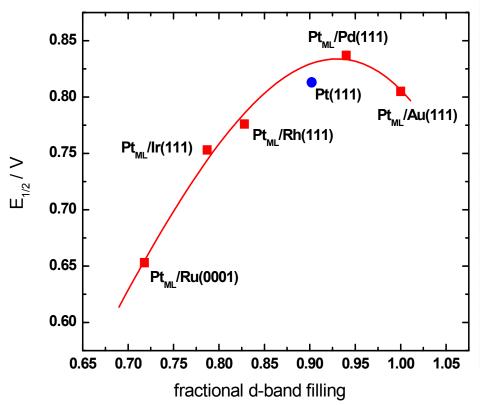
Wang et al. J. Phys. Chem., in press.



## O<sub>2</sub> REDUCTION ON Pt<sub>1ML</sub>/Pd(111)

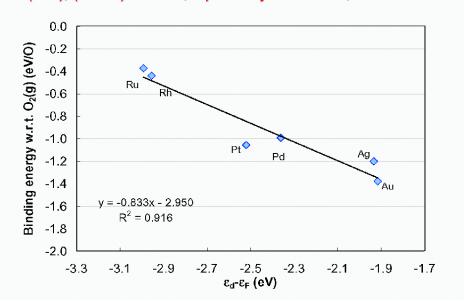


# ACTIVITY OF Pt MONOLAYERS AS A FUNCTION OF THE FRACTIONAL FILLING OF THE d-BAND OF SUBSTRATES



# Adsorption energies of atomic oxygen on Pt monolayers vs. d-band centers

fcc(111); (2x2x4) unit cell; top two layers relaxed; PW91 functional

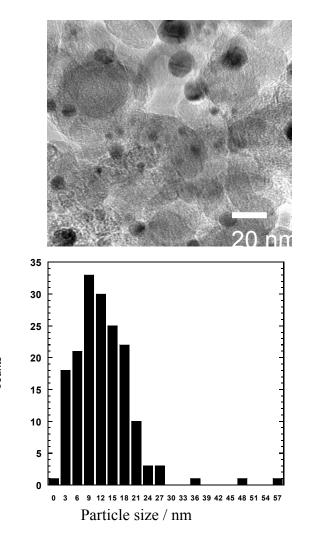


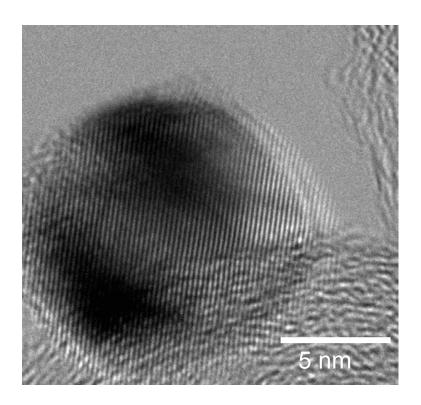
DFT calculations by M. Mavrikakis, U. Wisconsin.





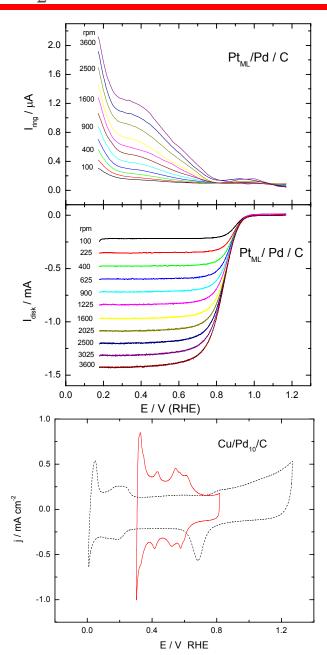
#### Pd(10%) / Vulcan XC-72 commercial

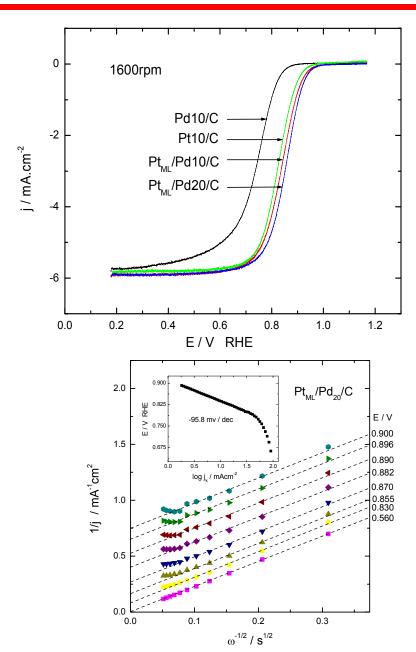




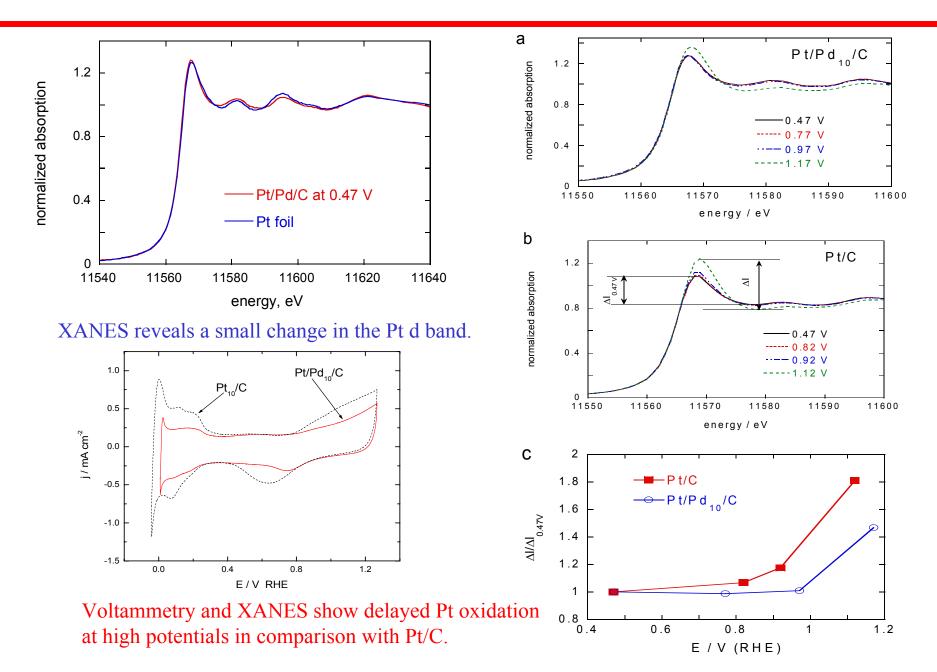


# O<sub>2</sub> REDUCTION ON Pt/Pd/C



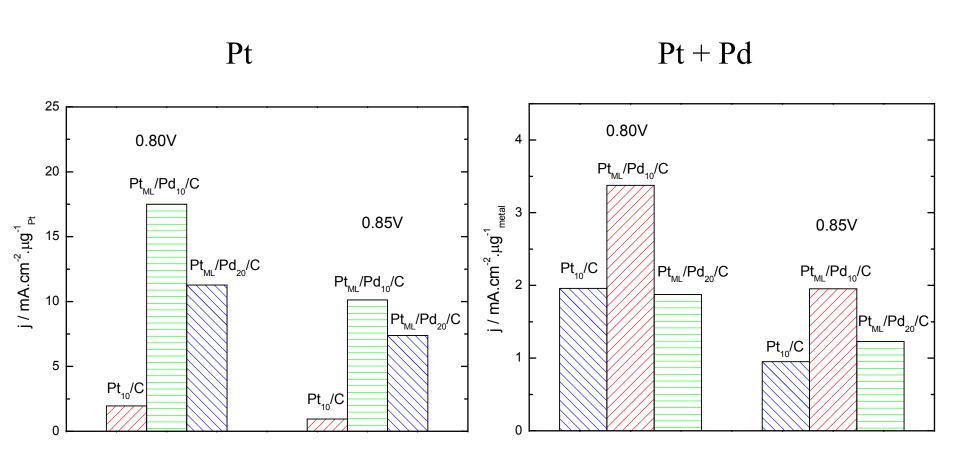






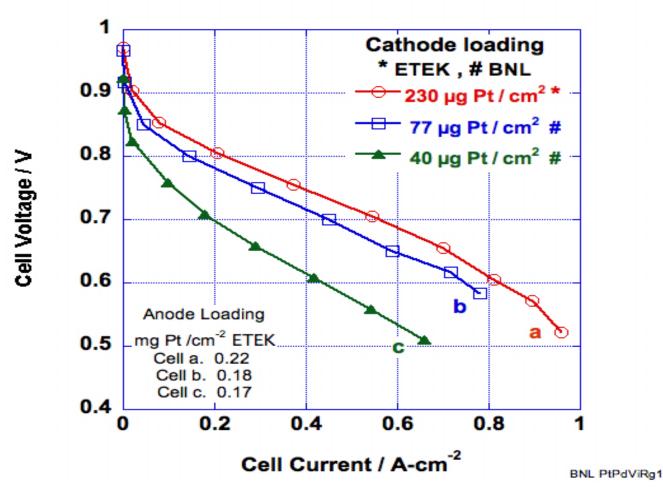


# Pt and (Pt + Pd) MASS-SPECIFIC ACTIVITY OF $Pt_{ML}/Pd/C$ FOR $O_2$ REDUCTION



#### FUEL CELL TESTS OF Pt/Pd/C AT LANL (F. Uribe)

#### Performance of Pt-Pd/C (BNL) cathode catalyst at 80 °C.

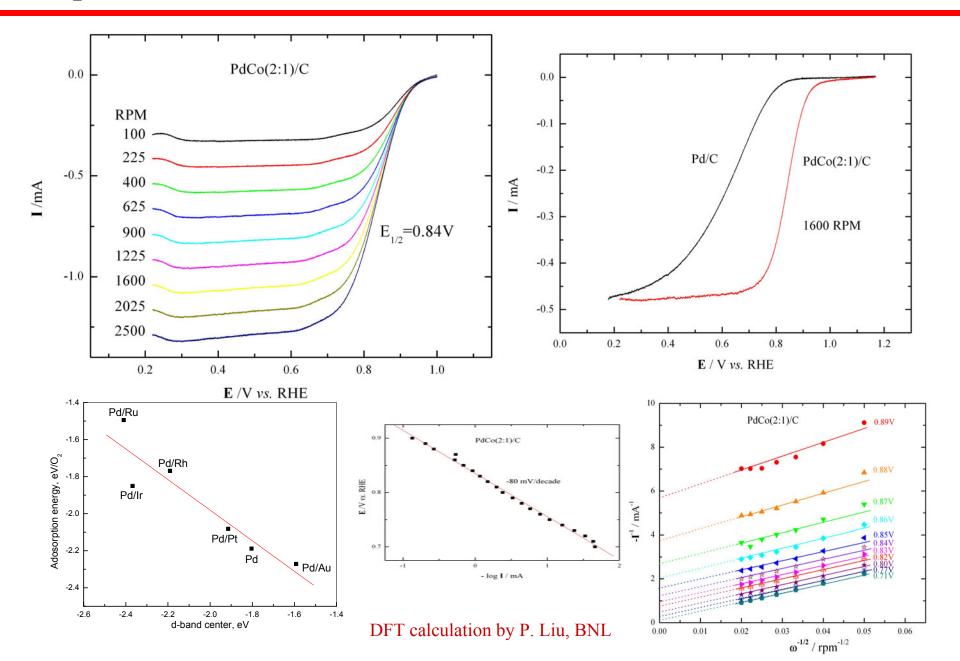


Performance of Pt-Pd/C (4% Pt-20% Pd) cathode catalyst at 80 °C. Membrane: Nafion® N1135.

Anode loadings in mg Pt/cm2: Cell **a:** 0.22 ; Cell **b:** 0.18 ; Cell **c**: 0.17.

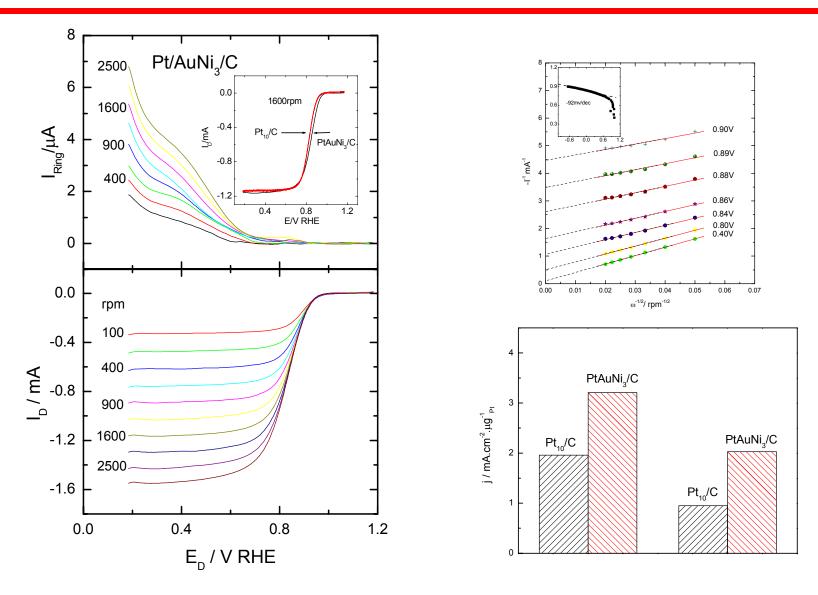
## O<sub>2</sub> REDUCTION ON PdCo/C





#### O<sub>2</sub> REDUCTION ON Pt/AuNi/C





Further reduction of Au and the use of an immiscible  $Au_{ML}Ni$  alloy seem possible.

#### INTERACTIONS AND COLLABORATIONS



- 1. Los Alamos National Laboratory Dr. Francisco Uribe longterm fuel cell tests of electrocatalysts.
- 2. Plug Power, visit, discussions.
- 3. Interest expressed in the PtRu<sub>20</sub> electrocatalyst and collaboration.

#### Publications from collaborations:

K. Sasaki, J.X. Wang, M. Balasubramanian, J. McBreen, F. Uribe, R.R. Adzic, Ultra-low Platinum Content Fuel Cell Anode Electrocatalyst with a Long-term Performance Stability, Electrochim. Acta, in press.

K. Sasaki, Y. Mo, J.X. Wang, M. Balasubramanian, F. Uribe, J. McBreen, R.R. Adzic, Pt submonolayers on metal nanoparticles – novel electrocatalysts for H<sub>2</sub> oxidation and O<sub>2</sub> Reduction, Electrochim. Acta, 48 (2003) 3841.

J.X. Wang, N.M. Markovic, R.R. Adzic, Kinetic Analysis of O<sub>2</sub> reduction on Pt(111) in Acid Solutions: Intrinsic Kinetic Parameters and Anion Adsorption Effects, J. Phys. Chem. in press.

#### BROOKHAVEN NATIONAL LABORATOR

#### Responses to Previous Year Reviewers' Comments

- Q. Distinction from Wieckowski's catalyst not clear.
- A. His: Ru on Pt for methanol oxidation; ours: Pt on Ru for  $H_2/CO$  oxidation.
- Q. Not clear how structure/phase behavior (of CO) is exploited to design practical catalysts.
- A. Knowing adsorbate's mobility, lateral interactions and adsorption sites can help in designing electrocatalysts.
- Q. Cathode materials of higher importance and needs to be expanded.
- A. The work on cathode materials has been expanded.

#### FUTURE WORK



### H<sub>2</sub> oxidation

1. Pt submonolayers on non-noble metal alloy nanoparticles.

#### O<sub>2</sub> reduction

- 1. Further development of a Pt/Pd/C electrocatalyst. Tests at LANL.
- 2. Further development of immiscible Au-non-noble metal alloy nanoparticles as support for Pt.
- 3. Multi-metal monolayers to reduce PtOH coverage and to modify the electronic properties of Pt.
- 4. Non-noble metal alloys as support for Pt.

